

*Idea will can fly when you ask why?*

# *PROCESS AND CONTROL LOOP CHARACTERISTICS*

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# PROCESS AND CONTROL LOOP CHARACTERISTICS

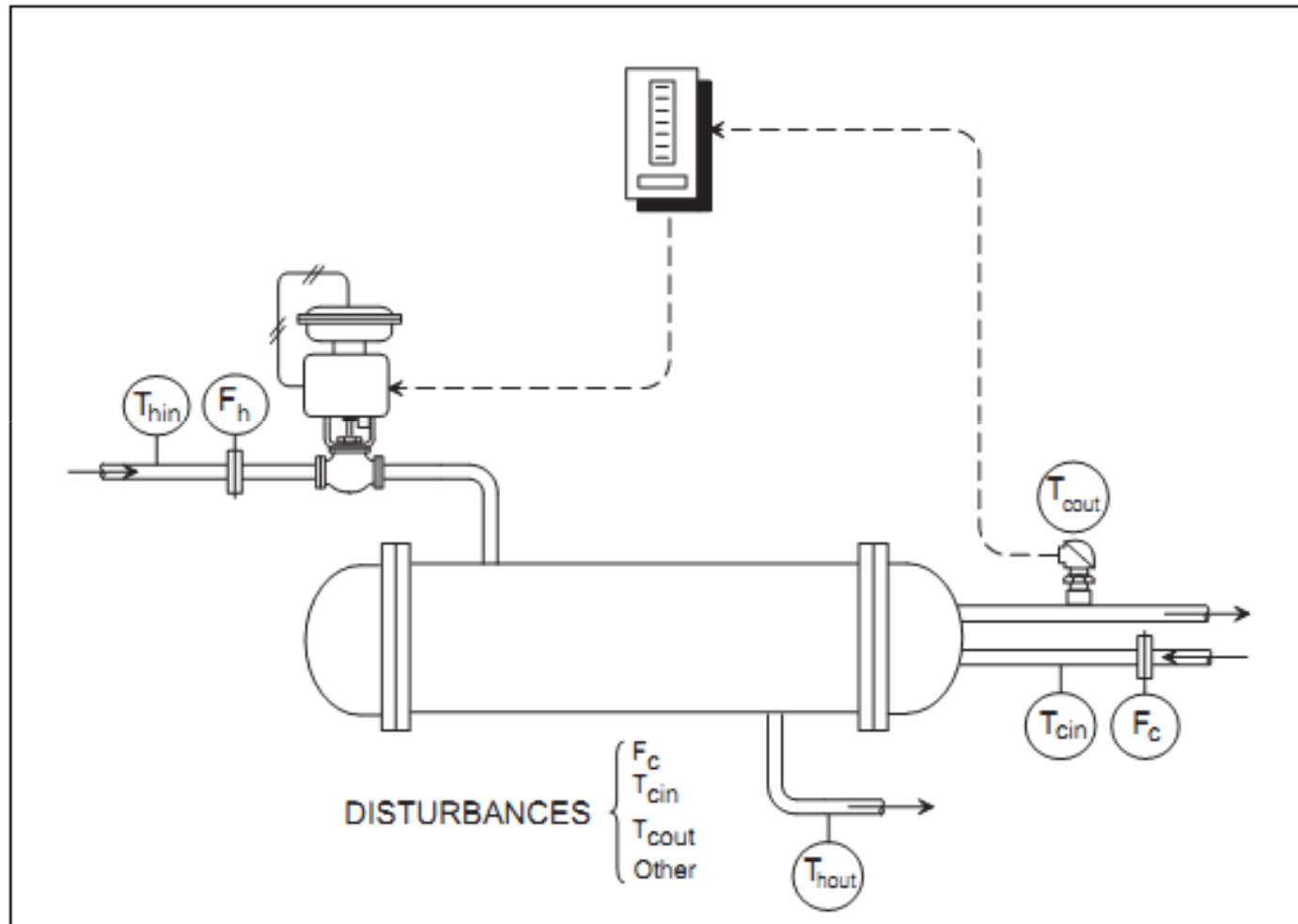


Figure 3-1. Disturbances to a Control Loop

## PROCESS AND CONTROL LOOP CHARACTERISTICS

- Changes in the process flow rate,  $F_c$ ;
- Changes in the process inlet temperature,  $T_{cin}$ ;
- Changes in the source temperature of the heating medium,  $T_{hin}$ ;
- Changes in the upstream or downstream pressure of the heating medium.  
(This would change the hot stream flow rate,  $F_h$ , even though the valve position did not change.)
- Scaling of the heat exchanger tubes—thus affecting the heat transfer coefficient; and
- Environmental effects, if the heat exchanger is not perfectly insulated.

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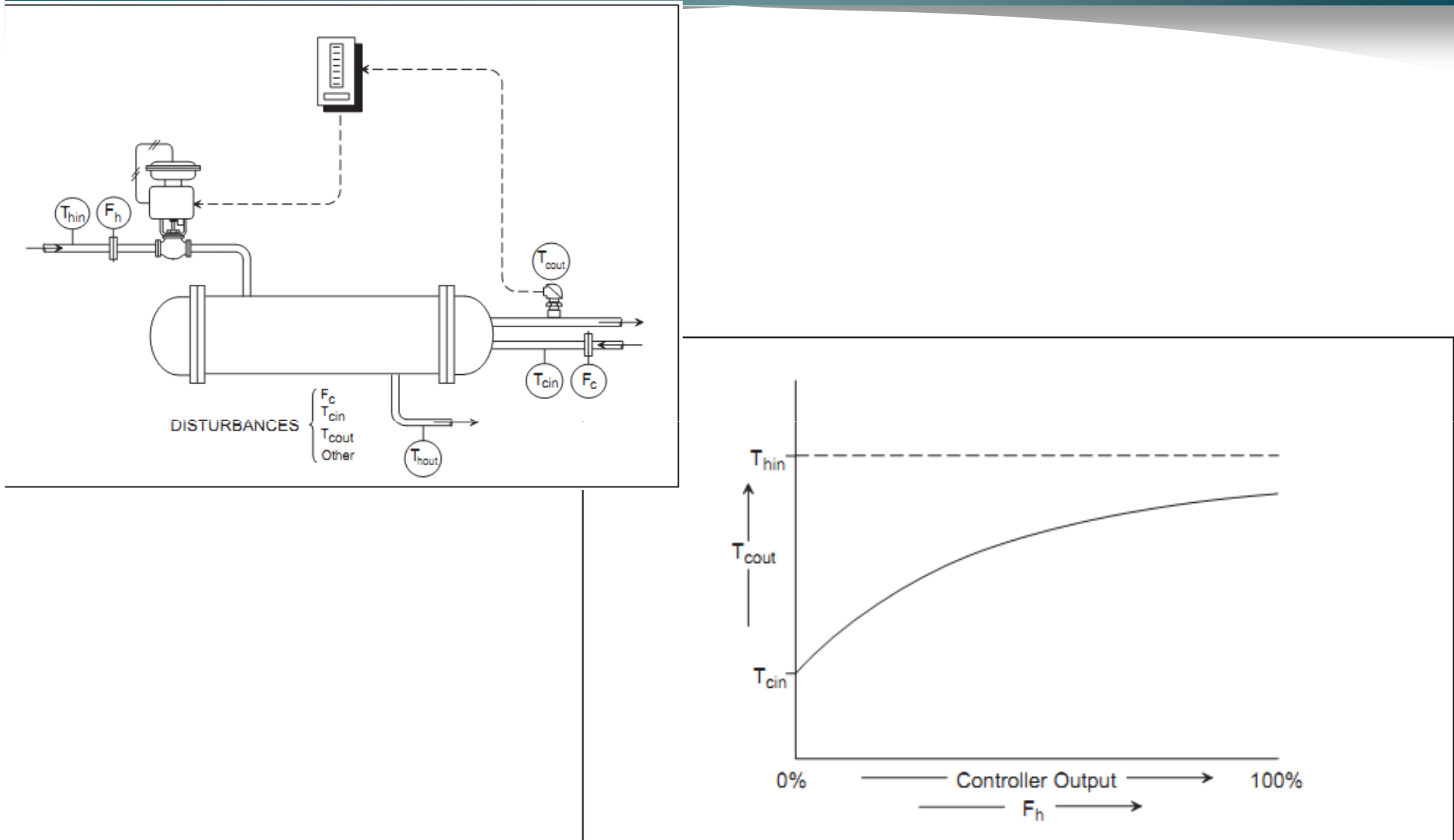


Figure 3-2. The Process Graph

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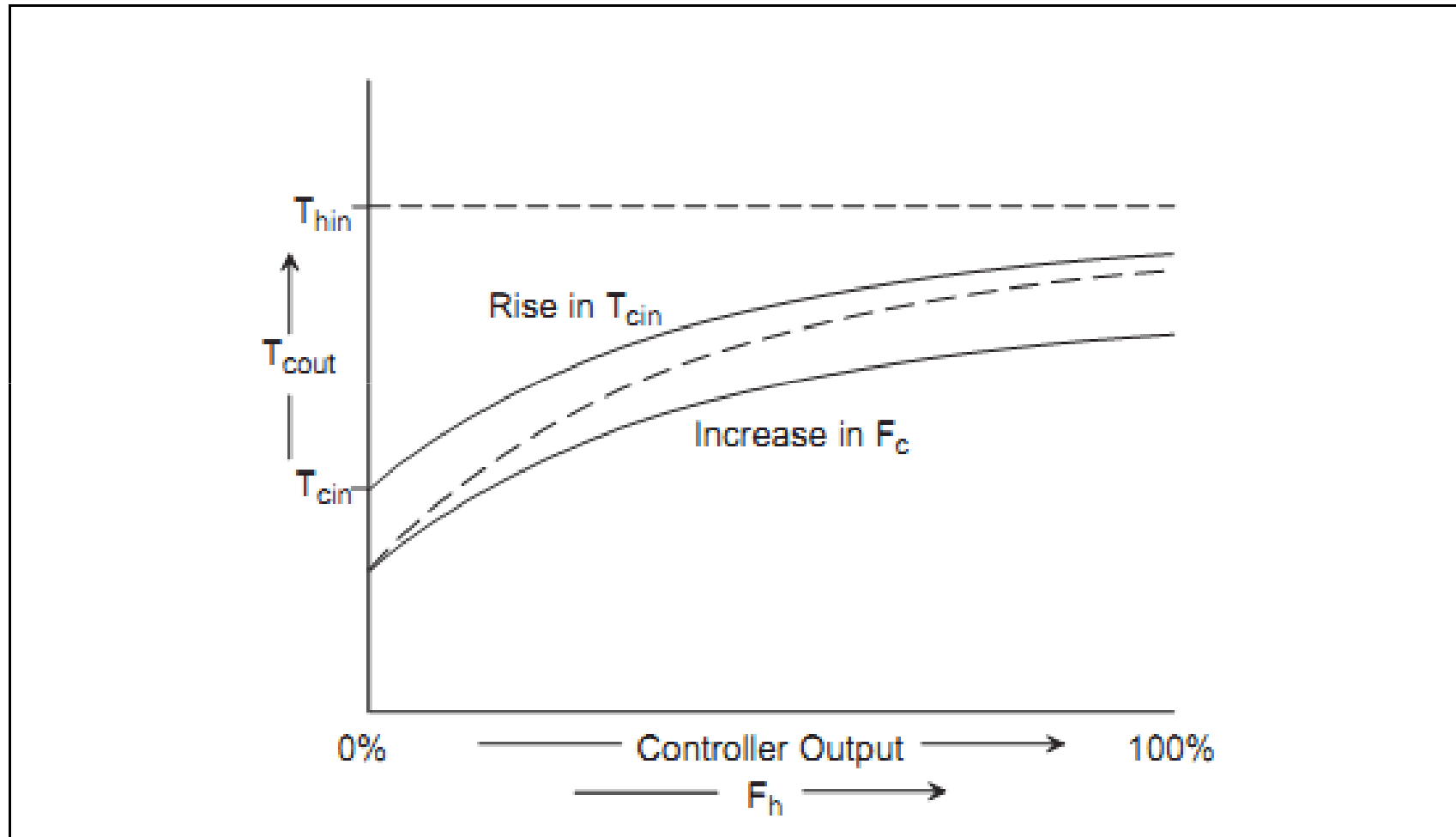


Figure 3-3. The Shifting of a Process Graph As a Result of Disturbances

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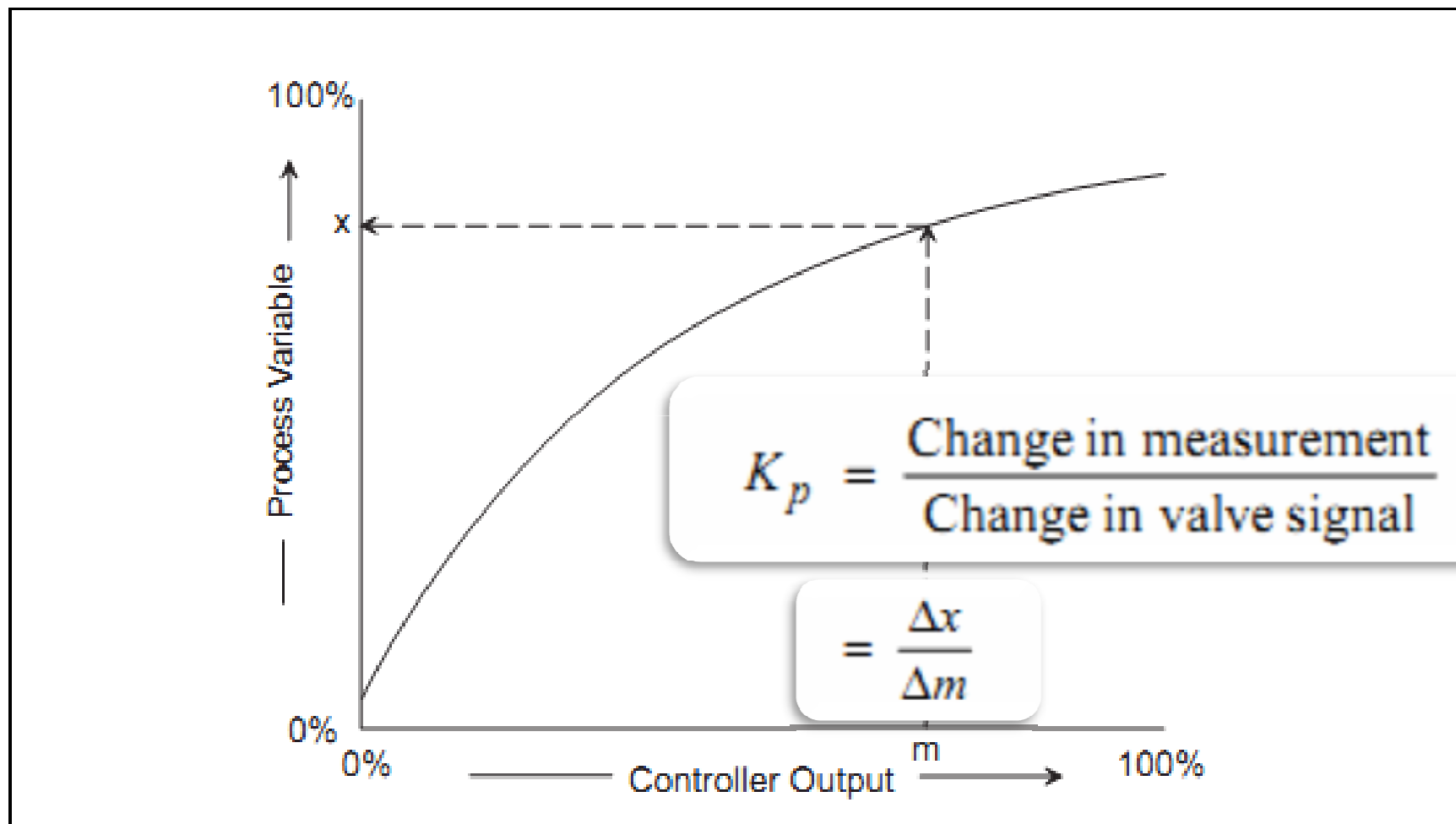
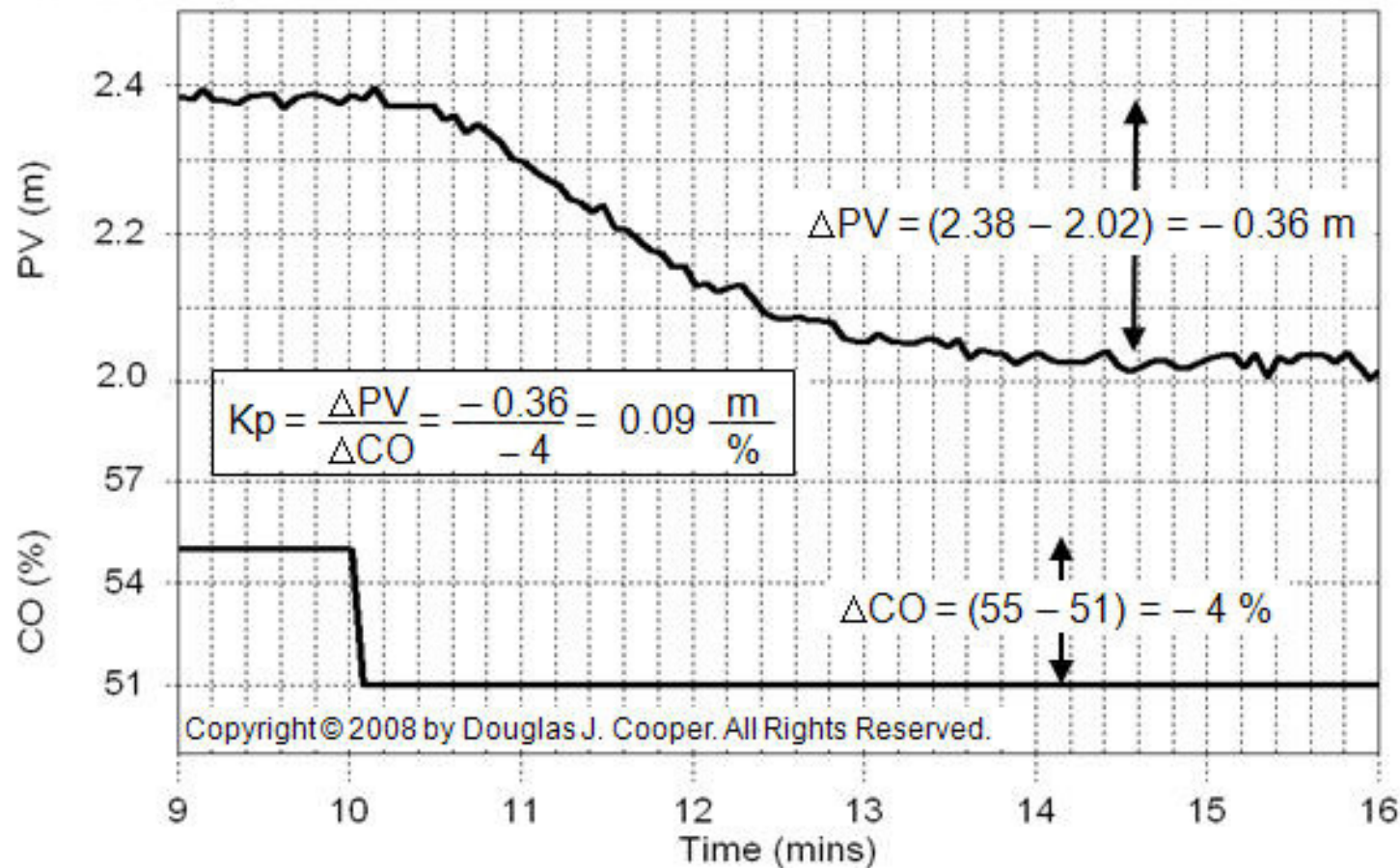


Figure 3-4. The Process Graph Determines the Controller Output Required to Bring the Measurement to a Desired Value

## Computing Process Gain, $K_p$ , from Step Test Data

Process: Gravity Drained Tank

Cont.: Manual Mode





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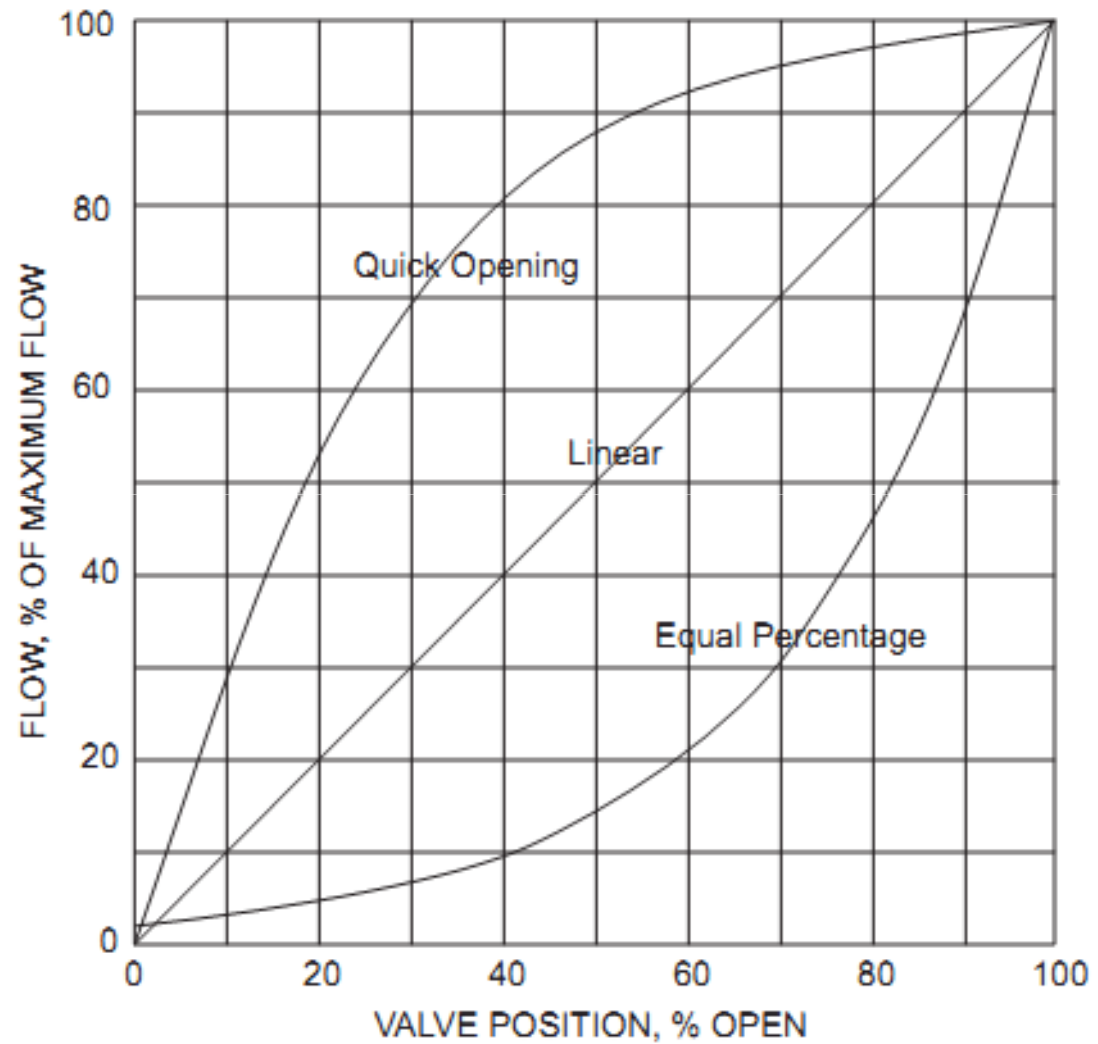


Figure 3-5. With Constant  $\Delta P$  across the Valve, Flow versus Valve Position Follows the Manufactured Characteristics



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$$\frac{\text{Minimum } \Delta P \text{ (when valve is wide open)}}{\text{Maximum } \Delta P \text{ (when valve is closed)}}$$

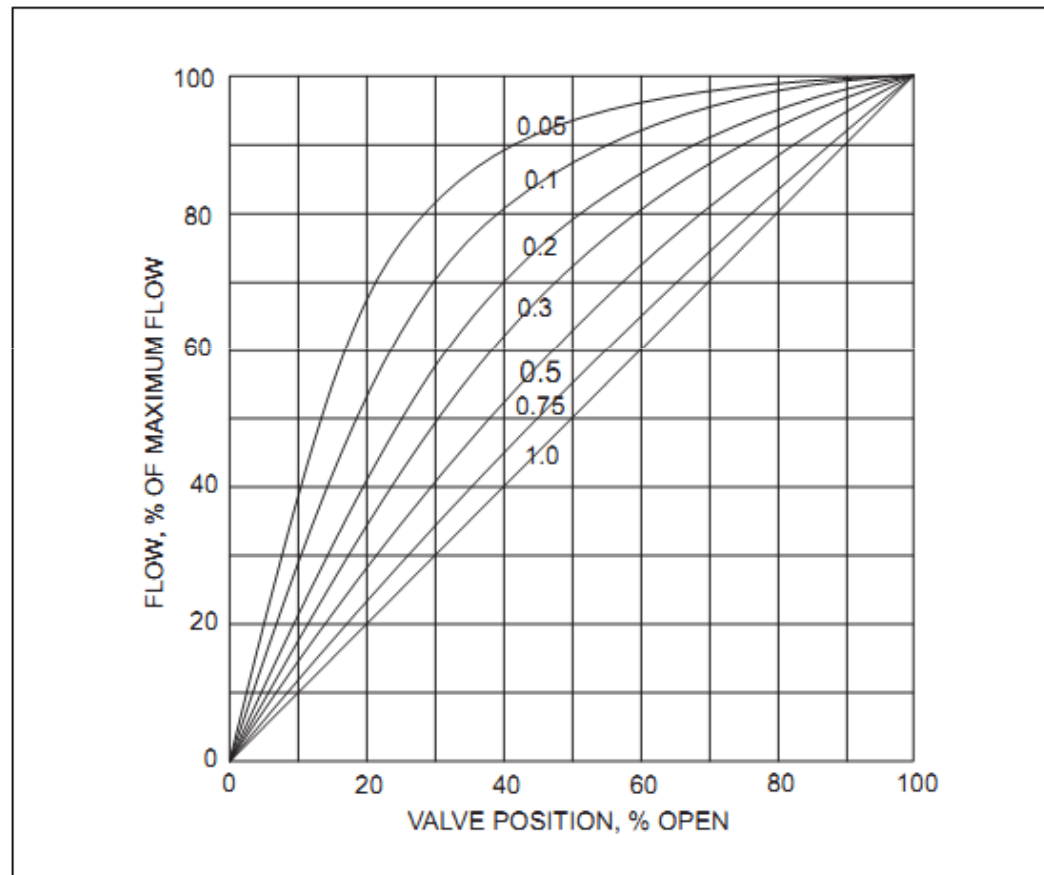
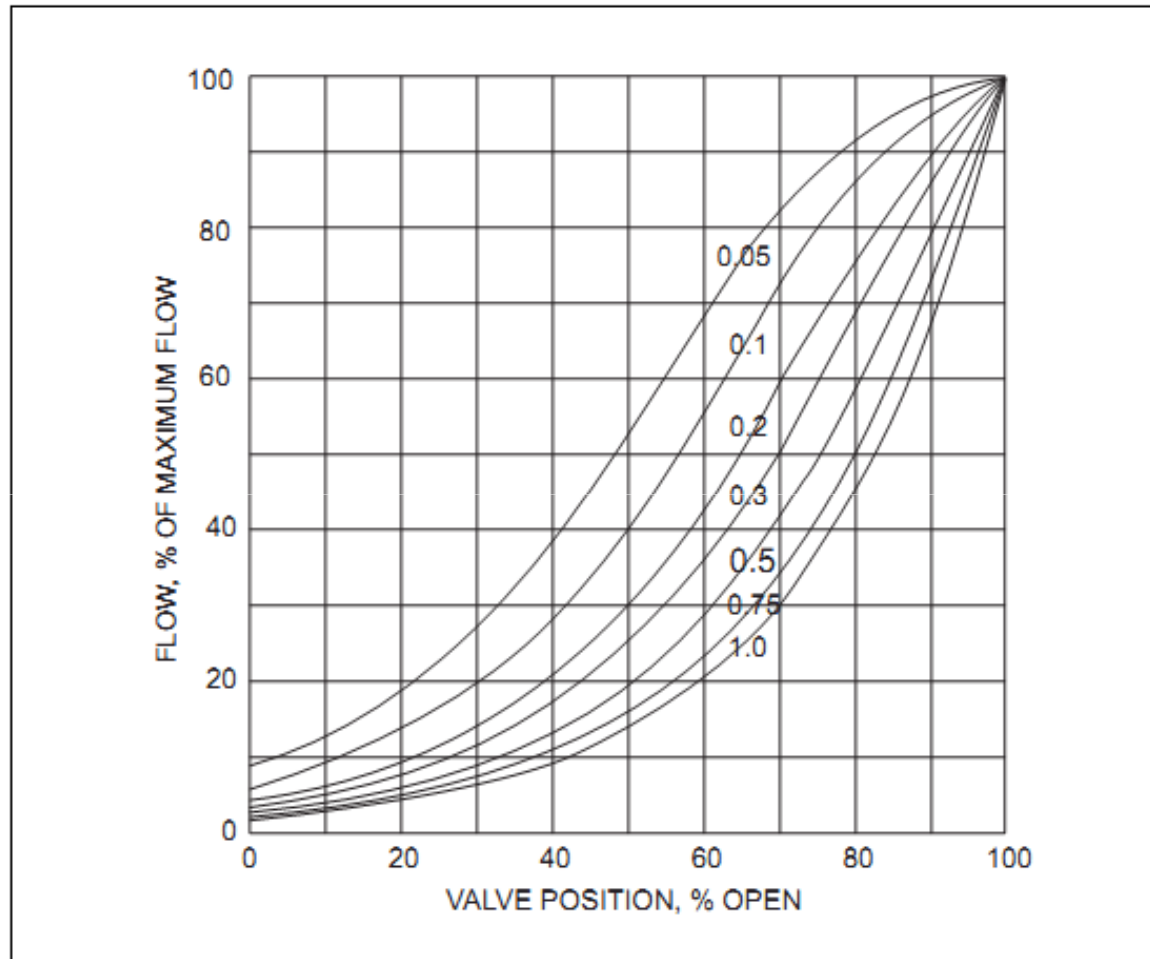


Figure 3-6. Installed Characteristics for a Linear Valve for a Range of Pressure Drop

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*Ratios:*  $\frac{\text{Minimum } \Delta P}{\text{Maximum } \Delta P}$

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## DYNAMIC CHARACTERISTIC

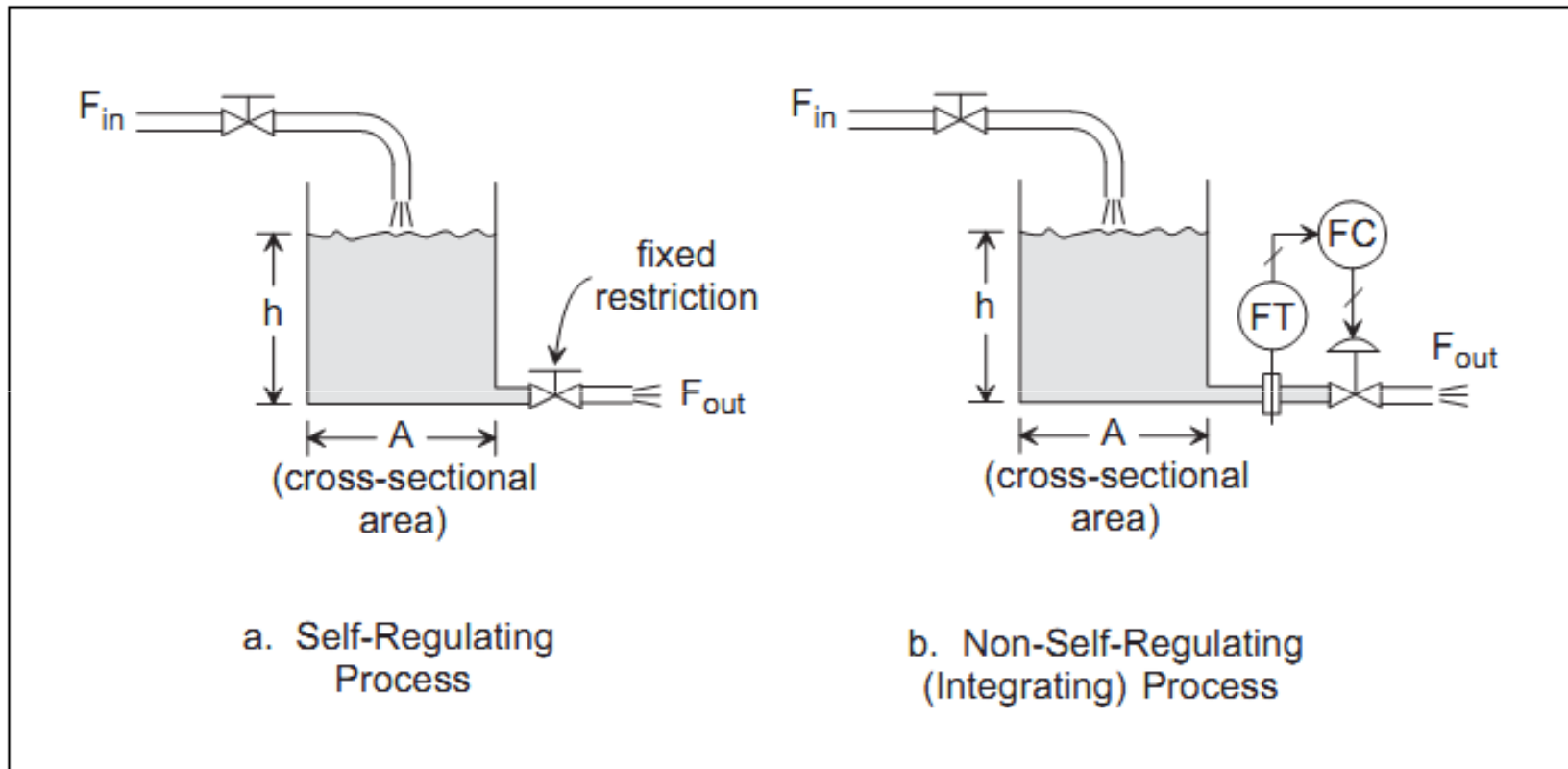


Figure 3-8. Hydraulic Analogies of Common Types of Process Characteristics

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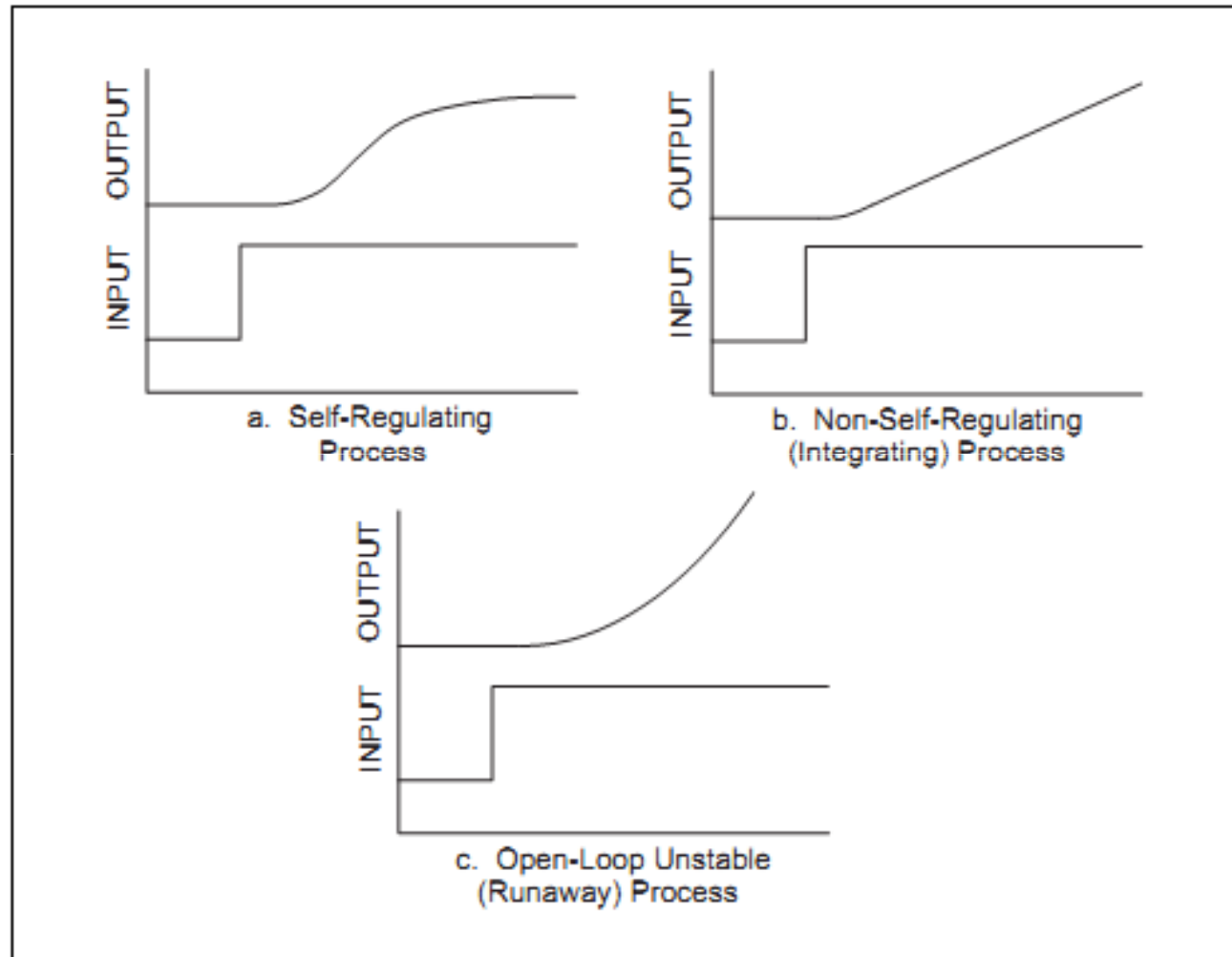


Figure 3-9. Step Input Response of Common Types of Process Characteristics

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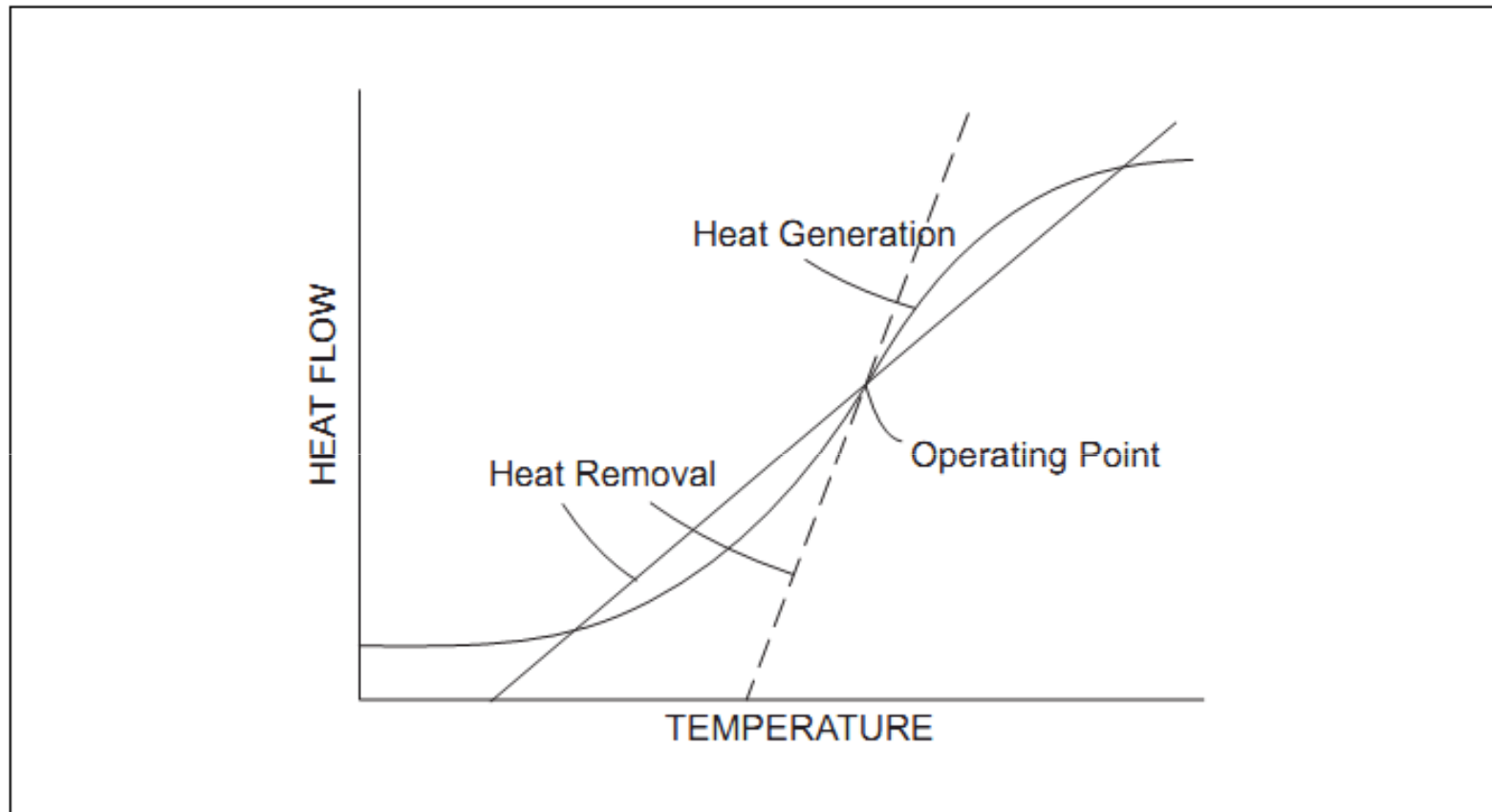


Figure 3-10. Heat Flow versus Temperature Curves for Exothermic Reactor

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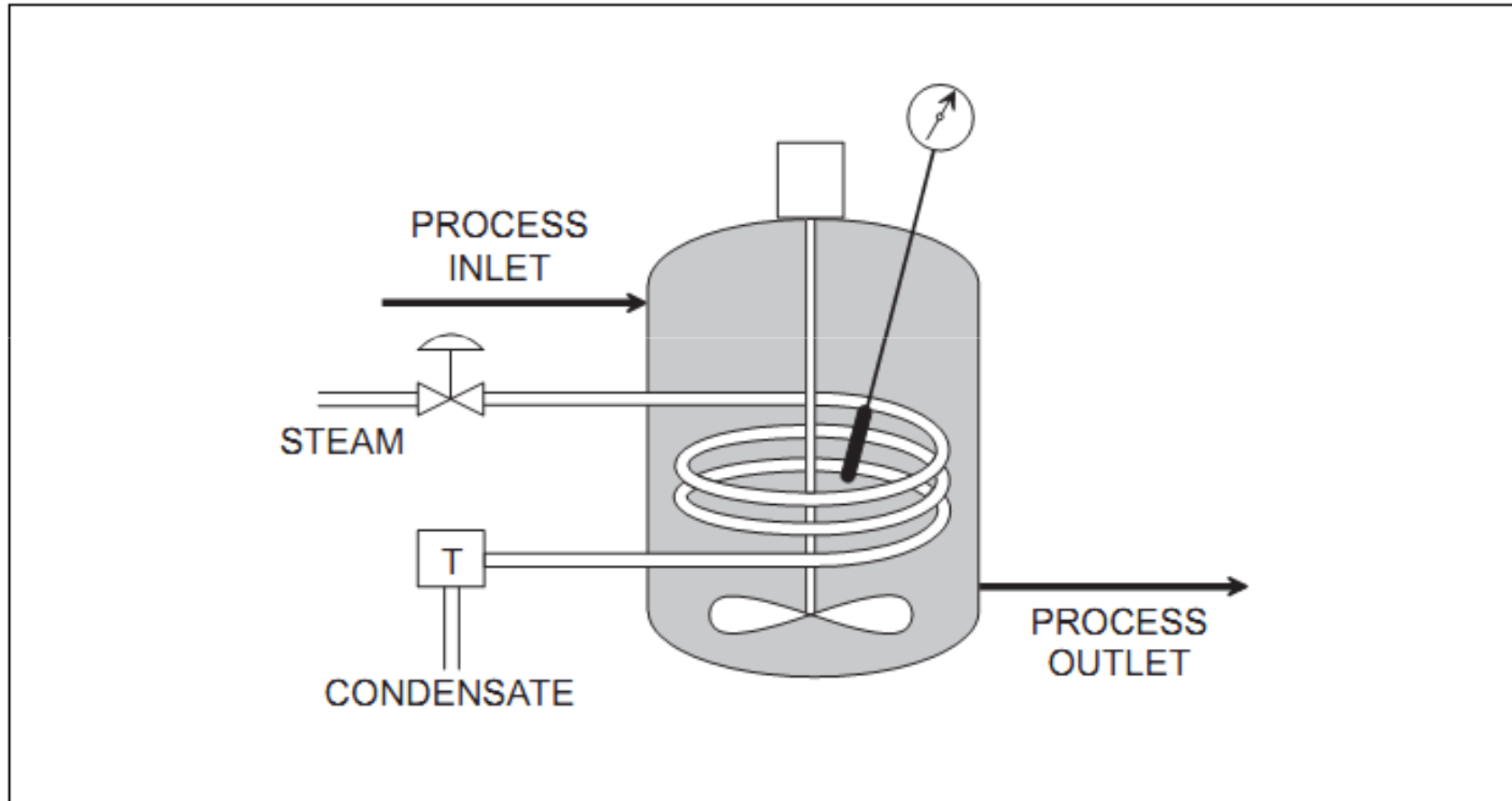
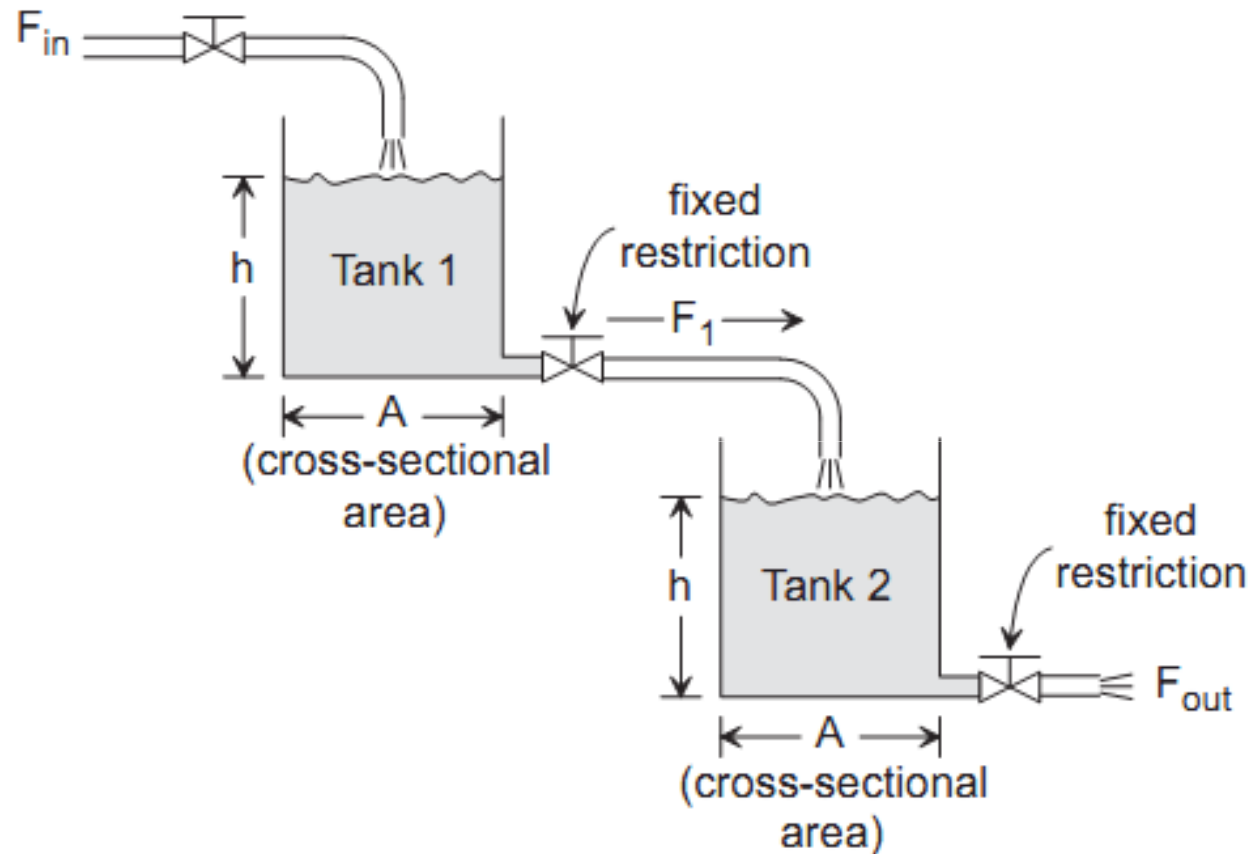


Figure 3-11. Process with Single Point of Energy Storage

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a. Uncoupled First-order Lags



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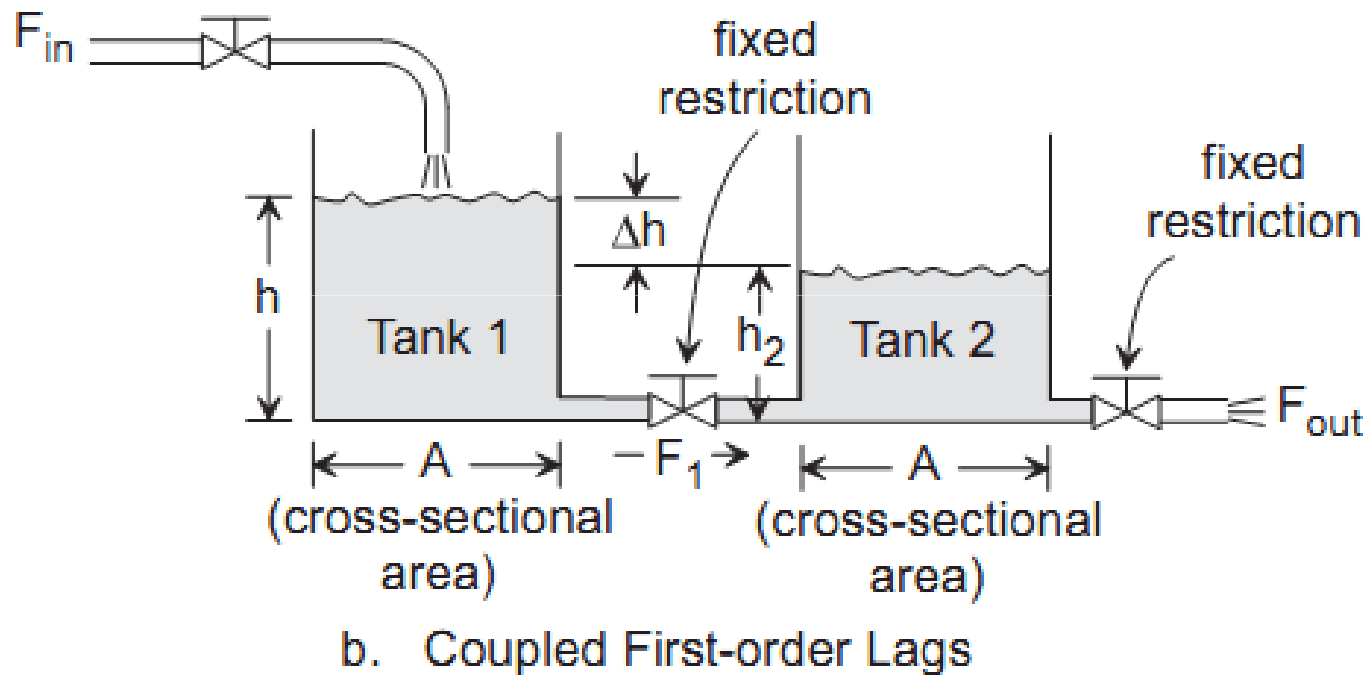


Figure 3-12. Hydraulic Analogies for Two Points of Mass Storage

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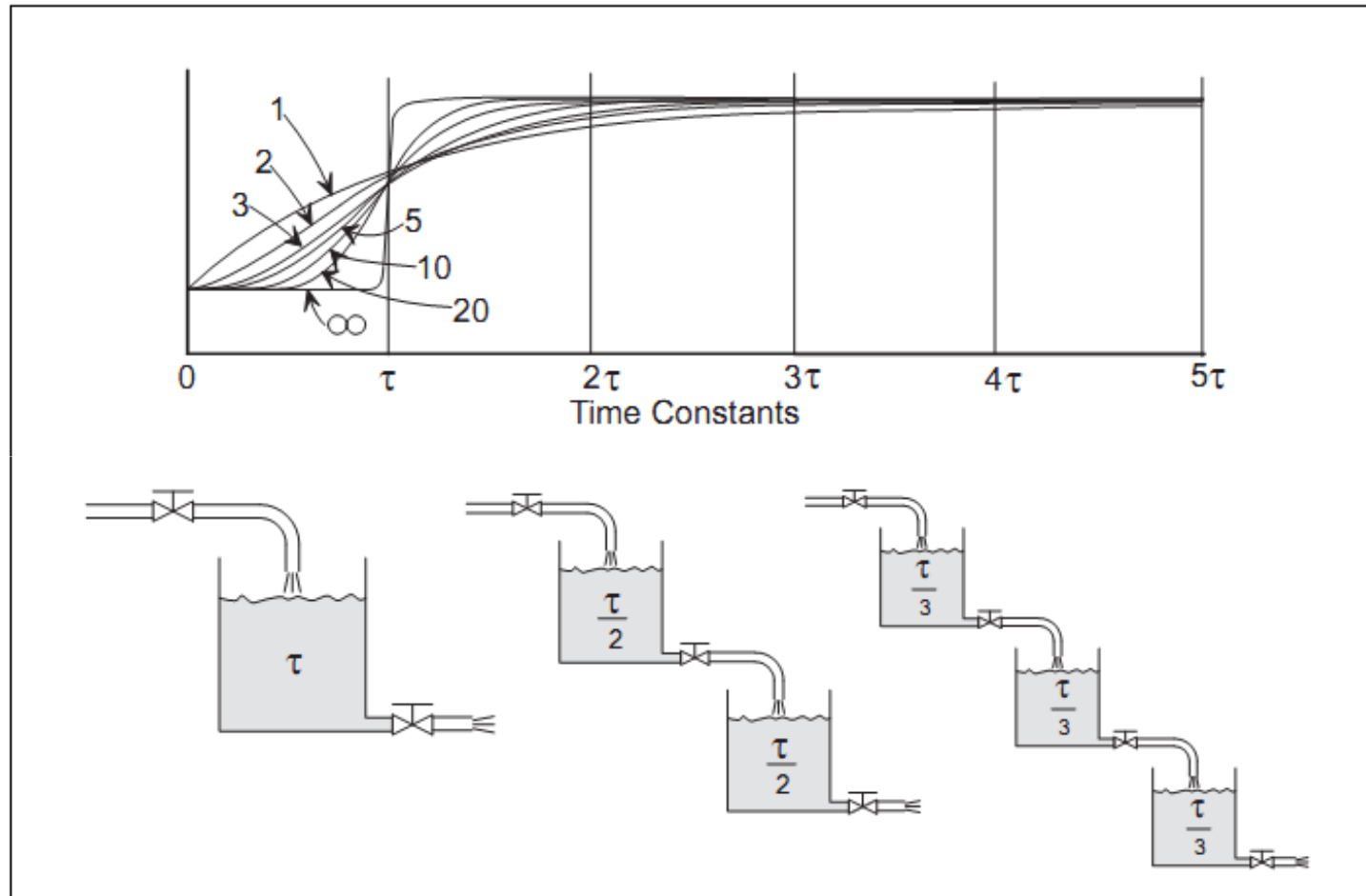


Figure 3-13. The Response of Multiple Uncoupled First-order Lags in Series

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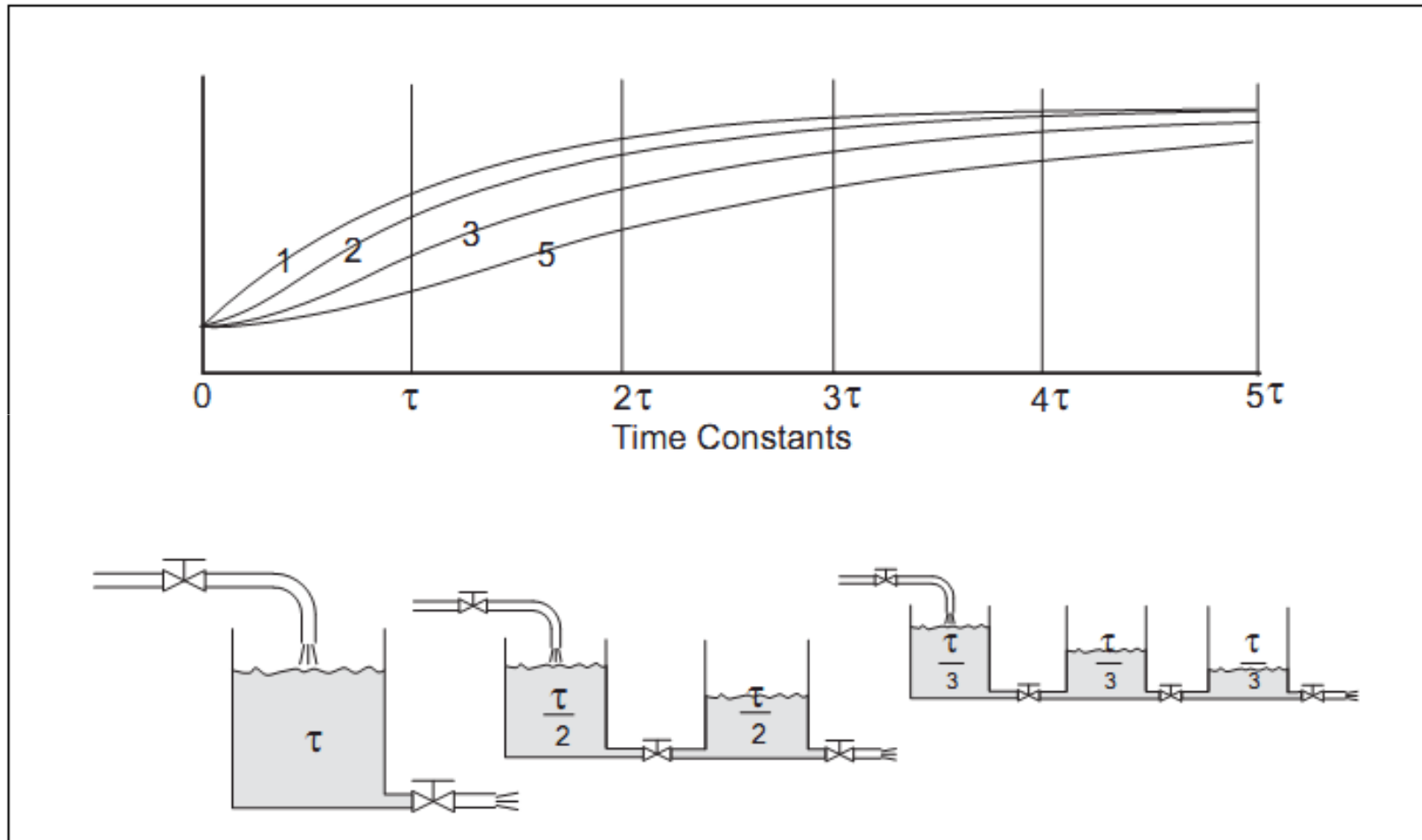


Figure 3-14. The Response of Multiple Coupled First-order Lags in Series

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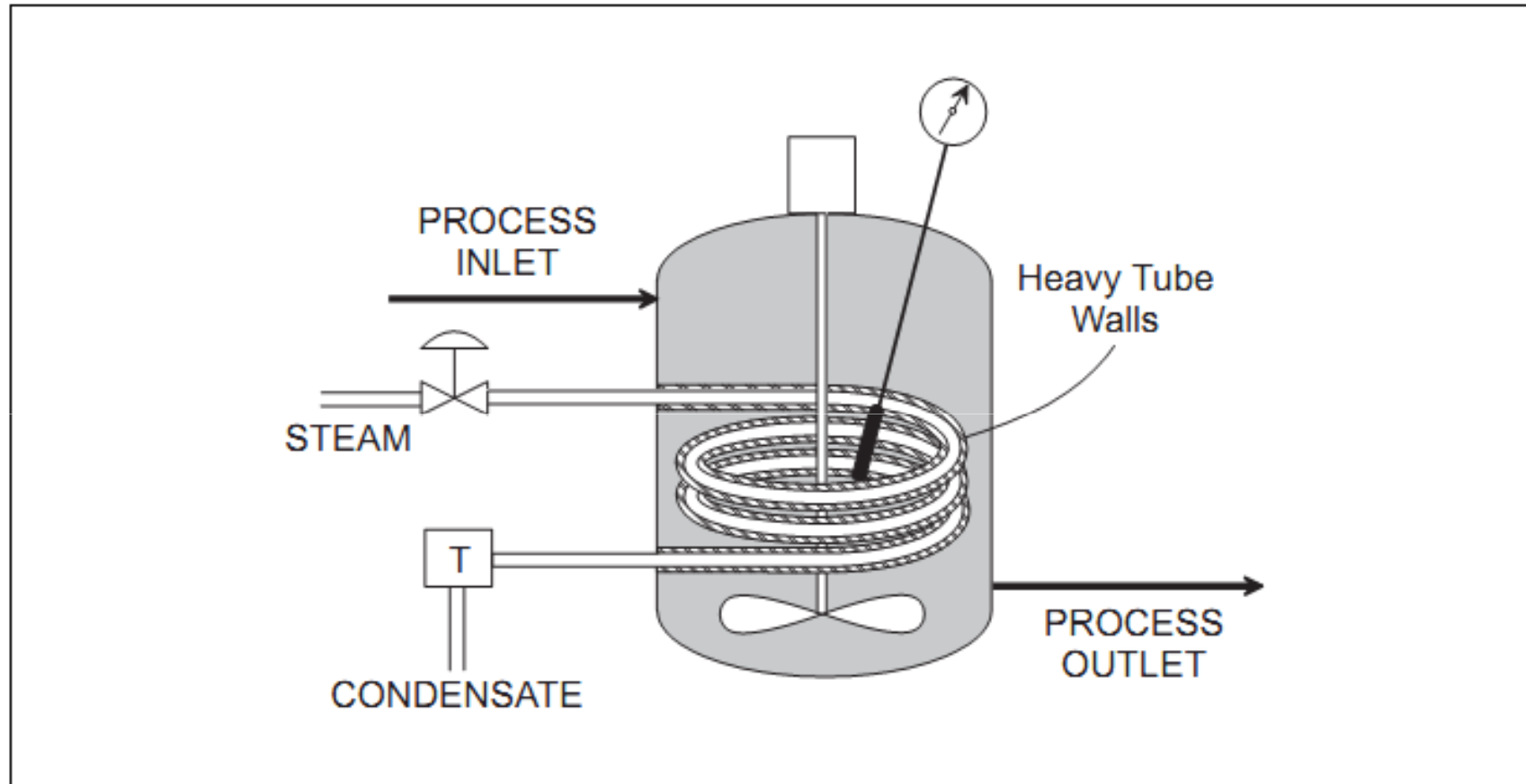


Figure 3-15. Example of Coupled First-order Lags

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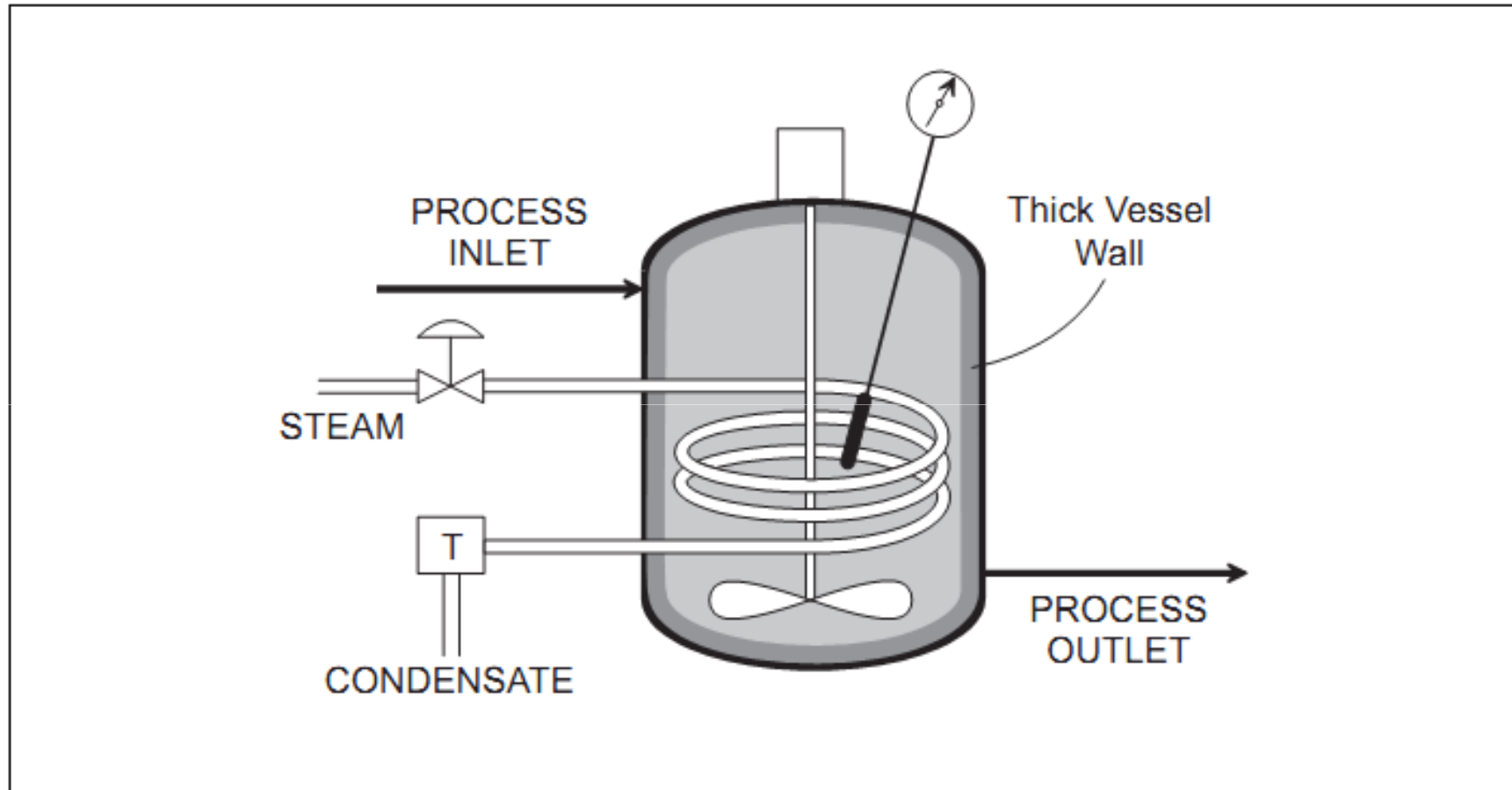


Figure 3-16. Example of Side Lag

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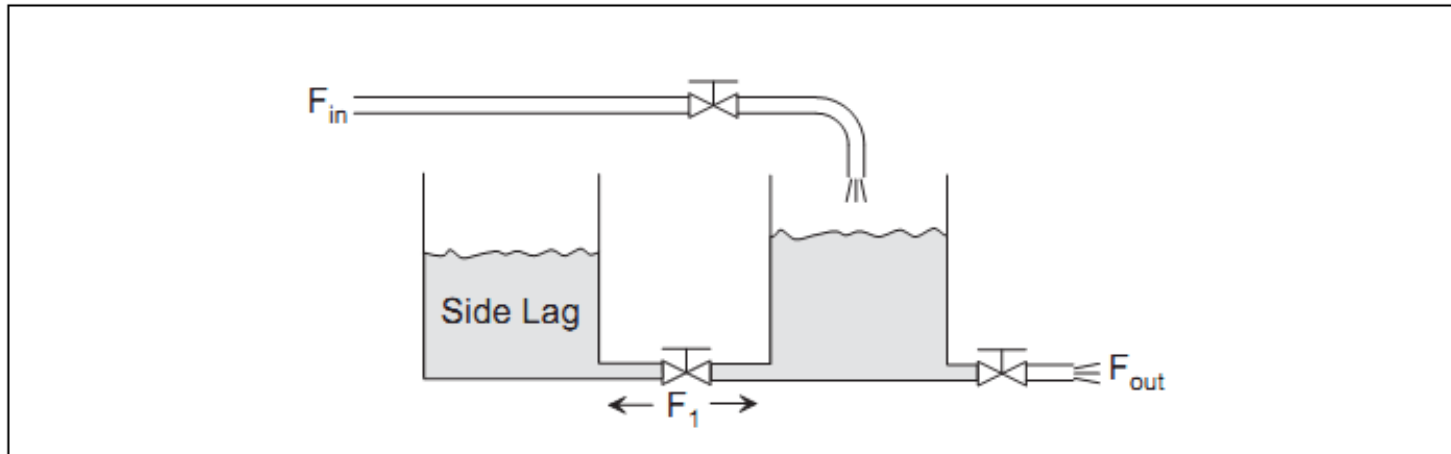


Figure 3-17. Hydraulic Analogy of Side Lag

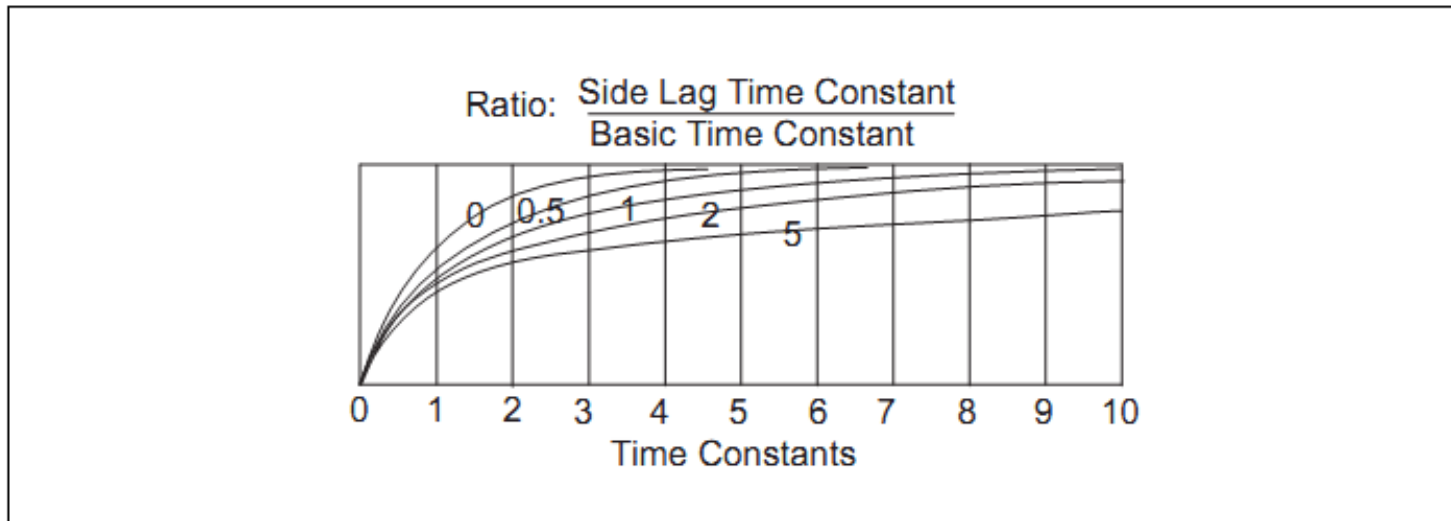


Figure 3-18. Response of Basic Lag Plus Side Lag

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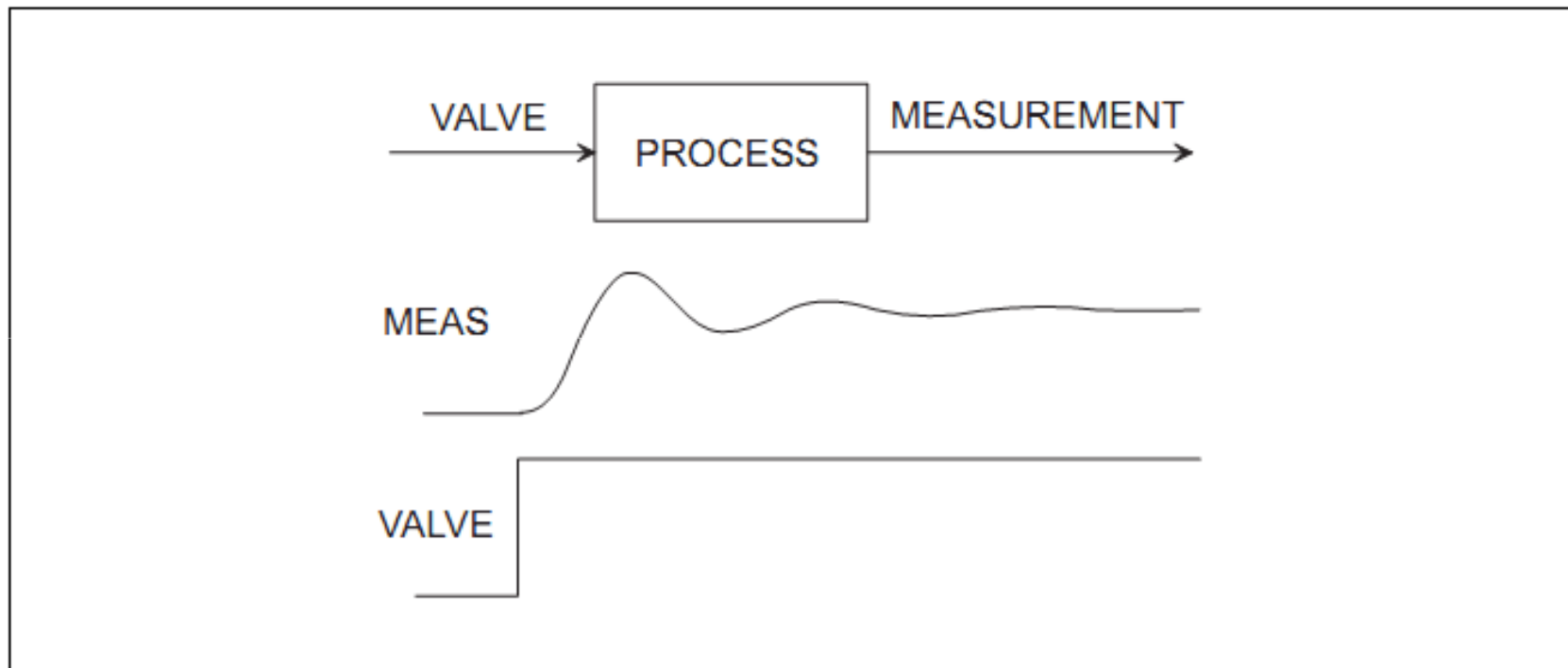


Figure 3-19. Open-Loop Response: Damped Oscillatory Behavior



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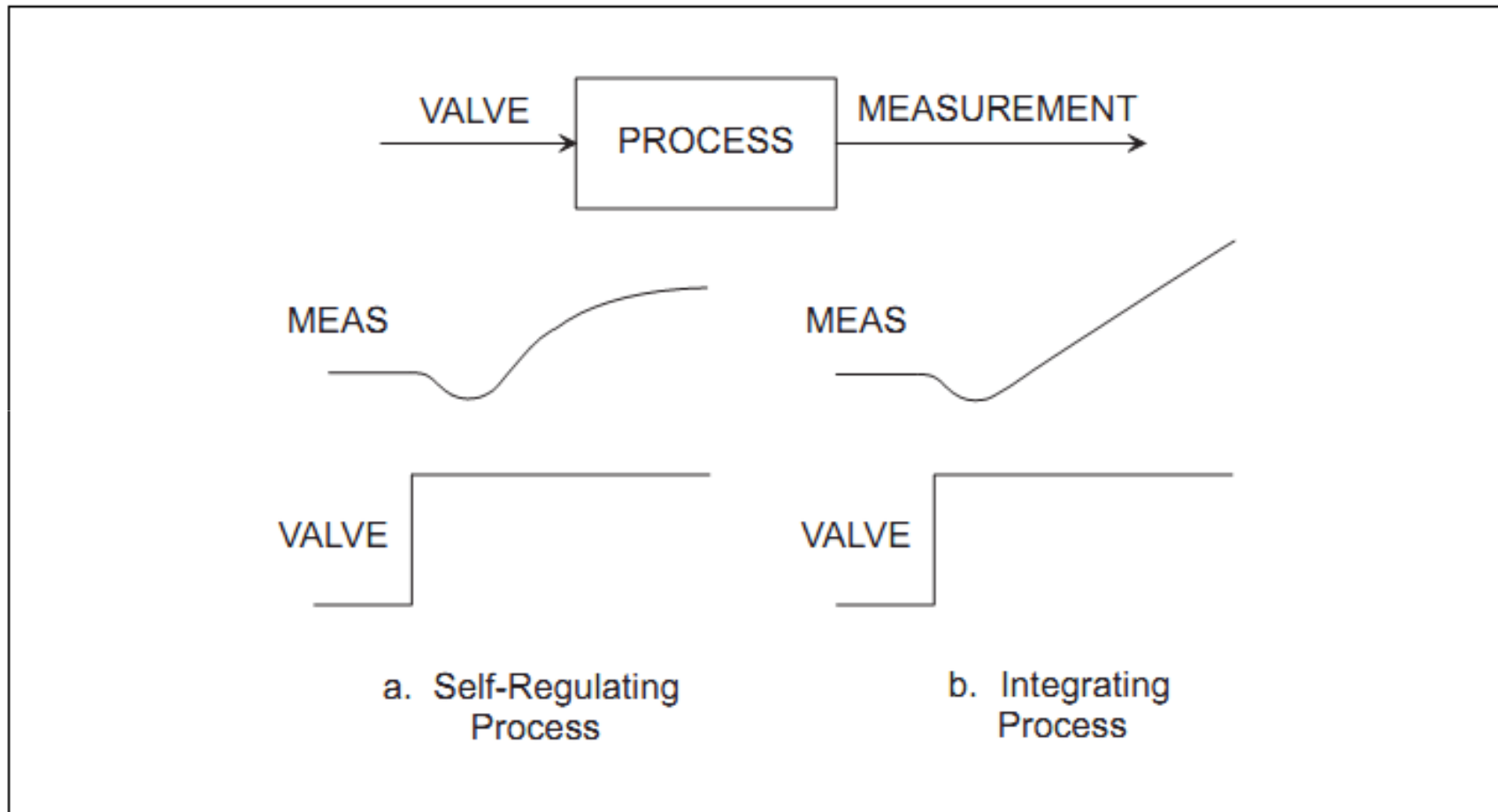


Figure 3-20. Inverse Open-loop Response

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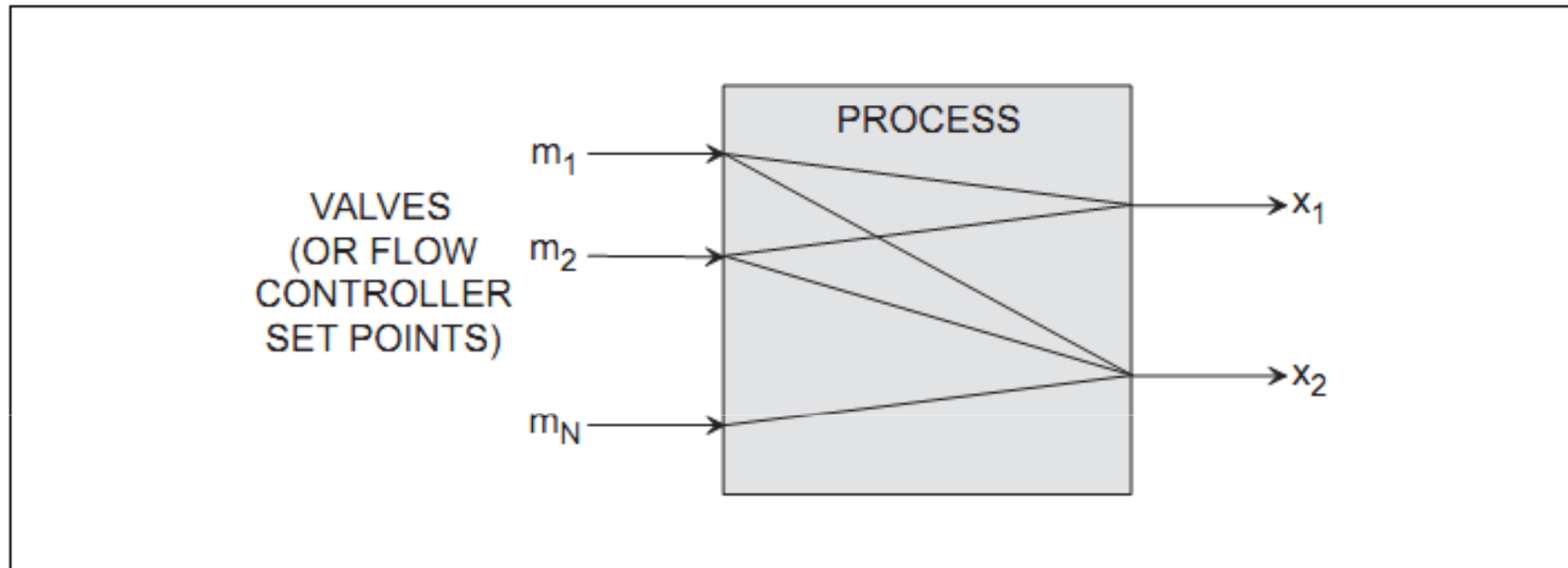


Figure 3-21. Multiple-Input, Multiple-Output Processes (Interacting Control Loops)

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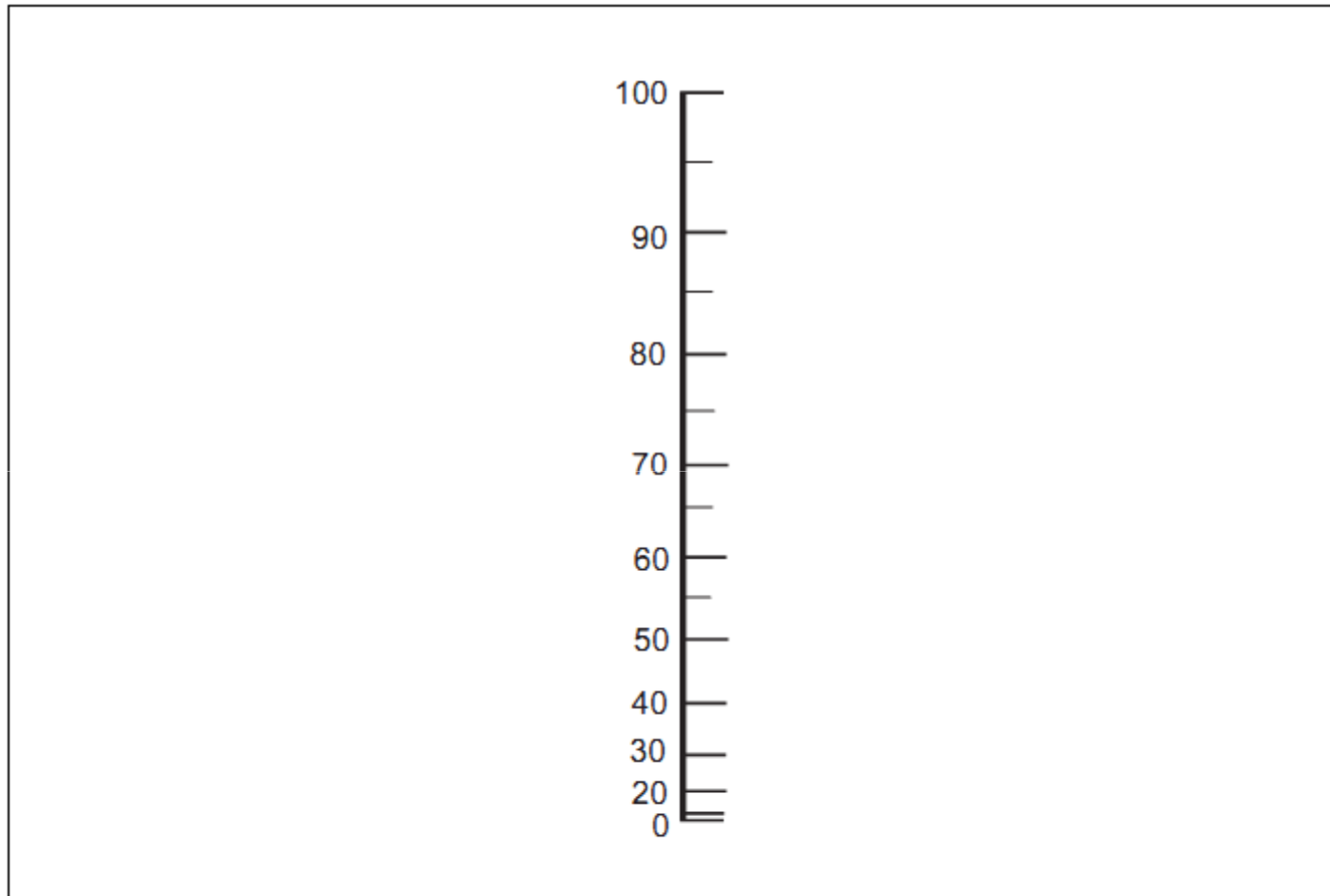
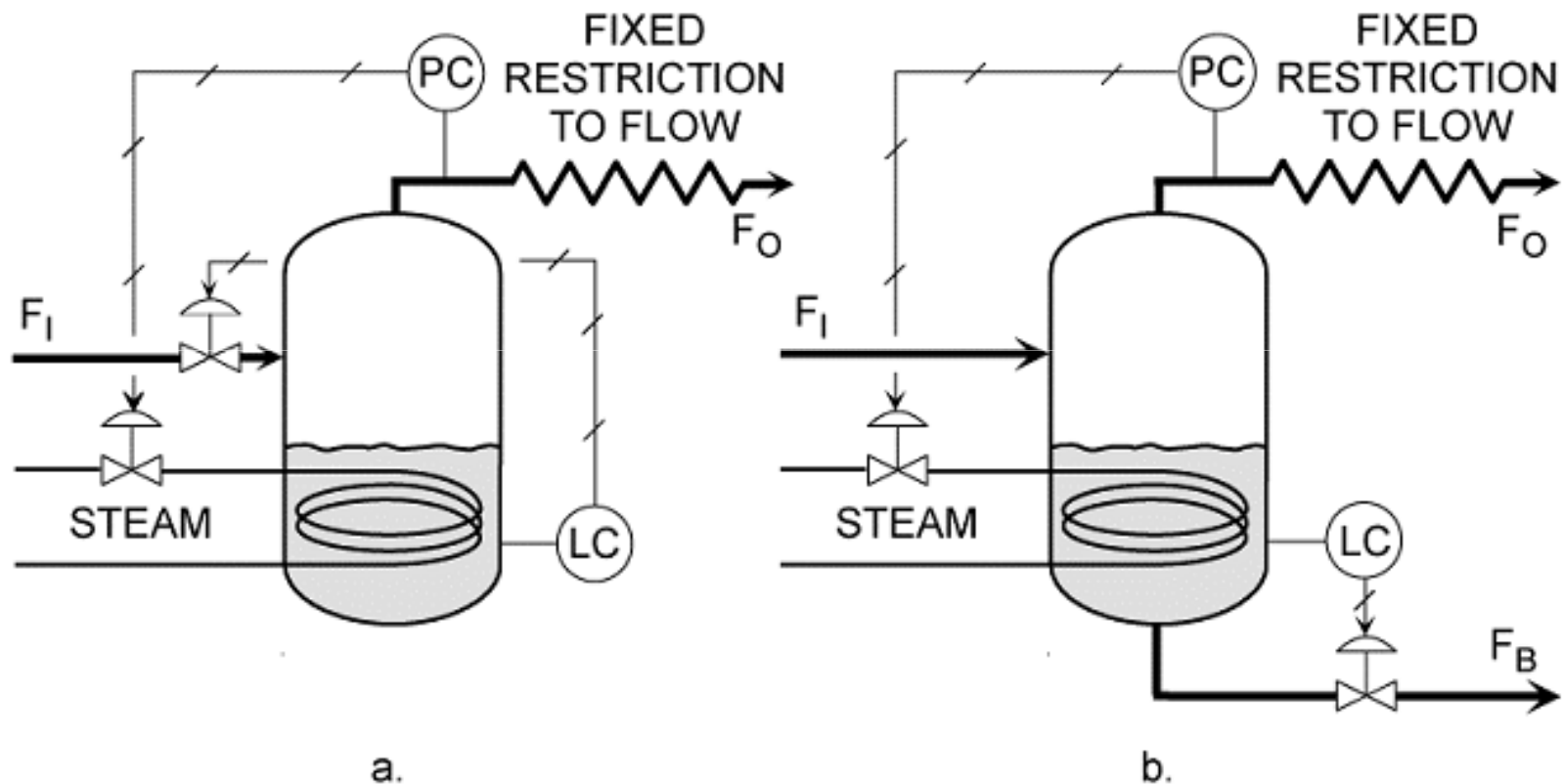


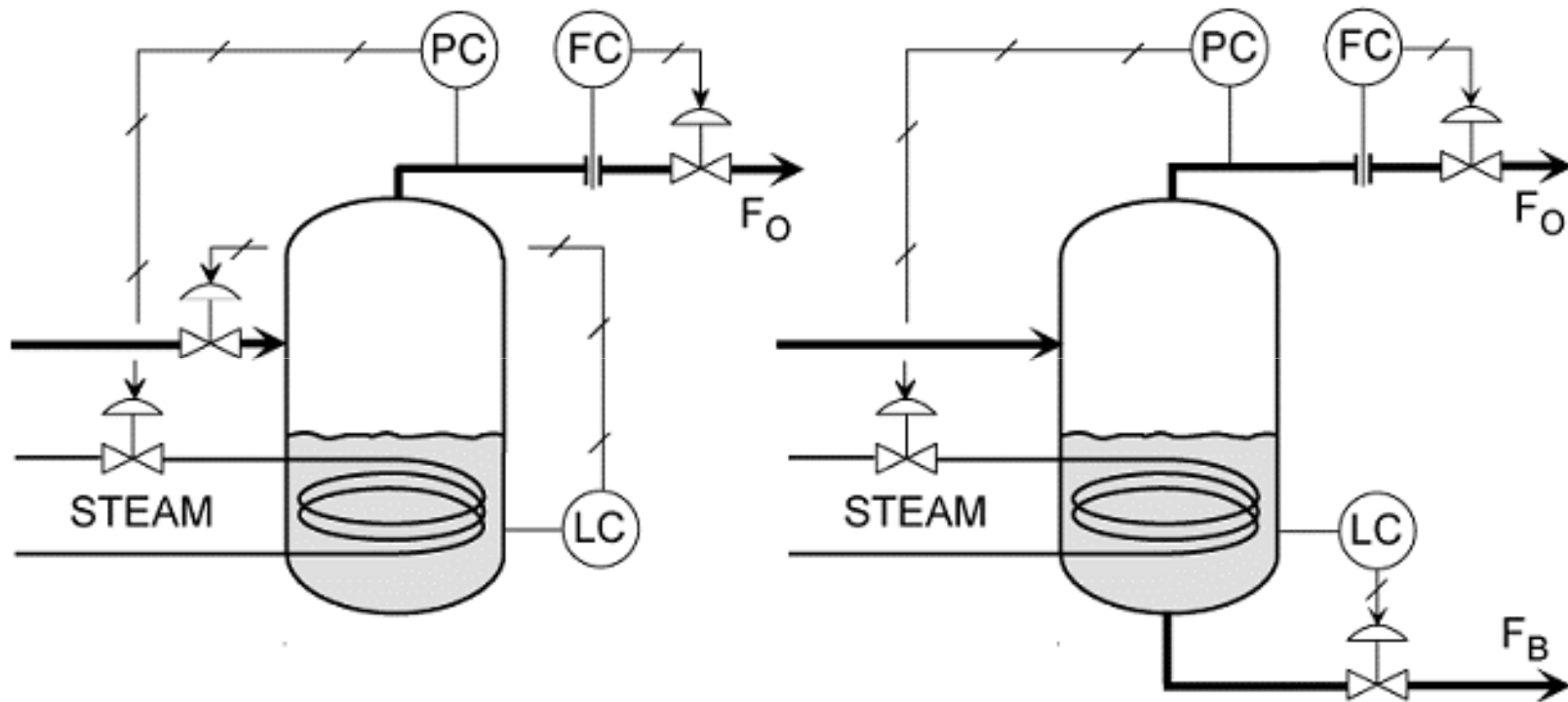
Figure 3-22. Nonlinear Display Scale When Flow Is Measured by a Differential Pressure Sensor without Square Root Extraction

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a. b.  
The Pressure Loop Controls a Self-Regulating Process

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c. d.  
The Pressure Loop Controls an Integrating Process



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